

Lithium-ion Insertion/Extraction Reaction with λ -MnO₂ in the Aqueous Phase

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The topotactic insertion of Li⁺ in λ -MnO₂ involved an evolution of oxygen and a reduction of Mn(IV) to Mn(III) in a (LiCl + LiOH) solution. The major reaction could be represented as λ -MnO₂ + xLiOH \rightarrow Li_xMnO₂ + (x/2)H₂O + (x/4)O₂, where x denotes moles of inserted Li⁺ per mole of λ -MnO₂. The extraction of the inserted Li⁺ was studied by using a solution containing either an acid(HCl) or an oxidizing agent(Br₂, K₂S₂O₈).

Recently, spinel-type manganese oxide(λ -MnO₂) has been prepared by extracting Li⁺ from LiMn₂O₄ with acid¹⁾ or an oxidizing agent.²⁾ Hunter proposed a disproportionation mechanism for the topotactic extraction of Li⁺ ($2\text{LiMn}_2\text{O}_4 + 4\text{H}^+ \rightarrow 3\lambda\text{-MnO}_2 + 2\text{Li}^+ + \text{Mn}^{2+} + 2\text{H}_2\text{O}$).¹⁾ Xiang-mu and Clearfield proposed an ion-exchange mechanism ($\text{LiMn}_2\text{O}_4 + \text{H}^+ \rightarrow \text{HMn}_2\text{O}_4 + \text{Li}^+$).³⁾ We have studied the insertion reactions of alkali metal ions with λ -MnO₂ in the aqueous phase.⁴⁾ The insertion reaction could scarcely proceed in a solution of each alkali metal chloride except Li⁺ ions, the insertion of which took place effectively only in the presence of OH⁻ ions. We explained the selective insertion of Li⁺ based on the "ion-sieve" effect of the tetrahedral vacant (or protonated) sites of the cubic closed-packed oxygen framework. The pH titration suggested a H⁺/Li⁺ ion-exchange mechanism for the Li⁺ insertion. However, we have found the evolution of oxygen and the reduction of Mn(IV) to Mn(III) during the Li⁺ insertion. In the present report, we will propose a redox mechanism for the major reaction of the topotactic insertion of Li⁺ in alkaline solutions.

λ -MnO₂ was prepared by the acid treatment of LiMn₂O₄.⁴⁾ The lithium content of the product(λ -MnO₂) was 0.29 mmol·g⁻¹, indicating that more than 92% of the lithium was extracted by the acid treatment. Metal ion insertion was carried out by mixing λ -MnO₂ with a (MCl + MOH, M = Li⁺, K⁺) solution at 25 °C. The concentrations of metal ions(Li⁺, K⁺, dissolved Mn) in the supernatant were determined by atomic absorption spectrometry and the OH⁻ concentration by titration with acid. The metal ion uptakes by λ -MnO₂ were calculated from the decreased metal ion concentrations and the amount of OH⁻ consumed from the decreased OH⁻ concentration. The evolution of gas was measured volumetrically in

a helium gas atmosphere at 25 ± 0.5 °C. The gas composition was analyzed by gas chromatography with ZSM5 packing. Extraction of Li^+ was carried out by mixing the Li^+ -inserted $\lambda\text{-MnO}_2$ with a solution containing 0.2-M HCl ($1 \text{ M} = 1 \text{ mol}\cdot\text{dm}^{-3}$), 0.1-M Br_2 , or 0.2-M $\text{K}_2\text{S}_2\text{O}_8$ at 25 °C.

The MnO_2 substances were analyzed for available oxygen, as well as Mn, Li^+ , K^+ , Cl^- , and water contents. The available oxygen was determined by the standard oxalic acid method.⁵⁾ After dissolving manganese oxide with a mixed solution of acid and H_2O_2 , the Li^+ , K^+ , and Mn contents were determined by atomic absorption spectrometry and the Cl^- content by ion chromatography. The water content was calculated from the weight loss by heating at 400 °C in air. The chemical composition was calculated according to a method described in the literature.⁶⁾ A powdered X-ray diffraction analysis was carried out.

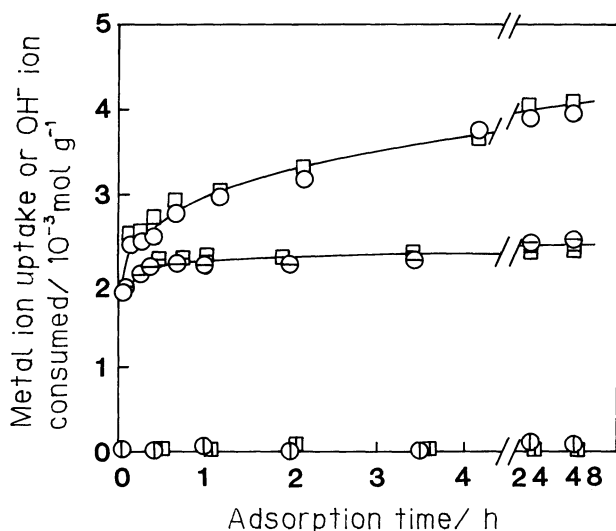


Fig. 1.

Time courses of metal ion insertion in $\lambda\text{-MnO}_2$ at 25 °C.

Circles and squares represent the amounts of metal ions inserted and OH^- consumed, respectively.

$\lambda\text{-MnO}_2$: 3.0 g,

volume of soln.: 300 cm^3 .

○ □: (0.1-M LiCl + 0.050-M LiOH)

⊙ ⊞: (0.1-M LiCl + 0.025-M LiOH)

⊙ ⊞: (0.1-M KCl + 0.025-M KOH)

The time dependences of Li^+ and K^+ insertions at 25 °C are illustrated in Fig. 1. In the case of a 0.025-M LiOH system, the insertion rate was relatively high; only 60 minutes was sufficient to reach 90% of the equilibrium uptake. In the case of a 0.050-M LiOH system, the insertion reaction was rapid up to a Li^+ uptake of 2.5 $\text{mmol}\cdot\text{g}^{-1}$, followed by a slow insertion phase. The amount of consumed OH^- was nearly equal to that of the inserted Li^+ over the insertion process. Supernatant solutions showed a slightly purplish color due to the presence of Mn(VII) ions. However, the concentration of Mn was less than 5×10^{-4} M. The equilibrium K^+ -uptake was very small (less than 0.2 $\text{mmol}\cdot\text{g}^{-1}$) compared to the Li^+ -uptake. The evolution of O_2 gas was observed in the case of Li^+ insertion (Fig. 2). The evolved amounts of the gas were found to be 0.57 and 0.84 mmol per gram of original $\lambda\text{-MnO}_2$ for 0.025-M LiOH and 0.050-M LiOH systems, respectively.

The X-ray diffraction analysis indicated that the crystal system of the metal ion-inserted sample was identical with that of $\lambda\text{-MnO}_2$. The lattice constant increased with the amount of inserted Li^+ (Table 1). A chemical analysis showed that most of manganese in $\lambda\text{-MnO}_2$ is in a tetravalent state. The Mn:O ratio scarcely changed through the insertion of Li^+ . This indicates a reduction of an equivalent amount of manganese from Mn(IV) to Mn(III) by Li^+ insertion. The Cl^- contents were less than 0.01 $\text{mmol}\cdot\text{g}^{-1}$ for all samples.

Table 1. Chemical Compositions and Lattice Constants

Sample	Chemical composition	Lattice constant(a_0)/nm ^f)
λ -MnO ₂	Li _{0.03} MnO _{2.0} (H ₂ O) _{0.05}	0.800
λ -MnO ₂ (Li-I) ^{a)}	Li _{0.25} MnO _{2.0} (H ₂ O) _{0.03}	0.811
λ -MnO ₂ (Li-II) ^{b)}	Li _{0.39} MnO _{2.0} (H ₂ O) _{0.02}	0.820
λ -MnO ₂ (K) ^{c)}	Li _{0.04} K _{0.005} MnO _{2.0} (H ₂ O) _{0.05}	0.800
λ -MnO ₂ (Li-Br ₂) ^{d)}	Li _{0.07} MnO _{2.0} (H ₂ O) _{0.05}	0.802
λ -MnO ₂ (Li-HCl) ^{e)}	Li _{0.07} MnO _{2.0} (H ₂ O) _{0.04}	0.802

- a) λ -MnO₂ was treated with a (0.1-M LiCl + 0.025-M LiOH) solution for 1 d.
 b) λ -MnO₂ was treated with a (0.1-M LiCl + 0.050-M LiOH) solution for 1 d.
 c) λ -MnO₂ was treated with a (0.1-M KCl + 0.025-M KOH) solution for 1 d.
 d) λ -MnO₂(Li-II) was treated with a 0.1-M Br₂ solution for 2 d.
 e) λ -MnO₂(Li-II) was treated with a 0.2-M HCl solution for 2 d.
 f) Lattice constant calculated from the X-ray diffraction pattern.

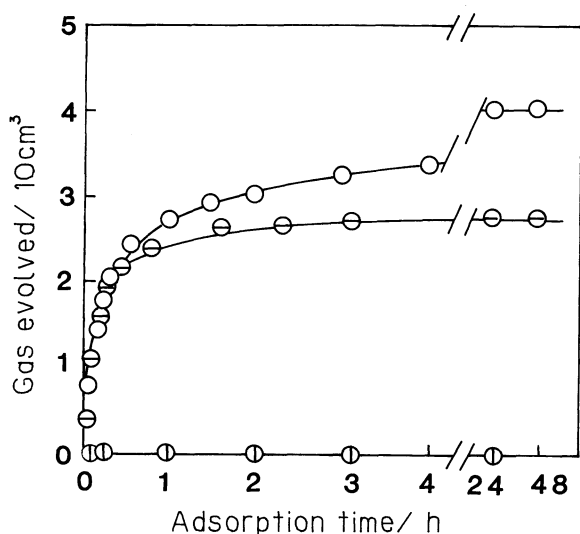


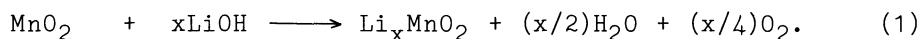
Fig. 2.

Time courses of gas evolution during the insertion of metal ions.

Suspension: 2 g λ -MnO₂ in 180 cm³ H₂O
 Volume of metal ion solution: 20 cm³

- : (1-M LiCl + 0.50-M LiOH)
 ◻: (1-M LiCl + 0.25-M LiOH)
 ⊙: (1-M KCl + 0.25-M KOH)

As a result of the above chemical analysis, the major reaction of the Li⁺ insertion could be represented by the following chemical reaction using symbol x, moles of inserted Li⁺ per mole of λ -MnO₂ (0 < x < 0.5):



The amounts of evolved O₂ (0.57 and 0.84 mmol·g⁻¹ for 0.025-M LiOH and 0.050-M LiOH systems, respectively) were about 85% of the expected values, 0.63 and 1.0 mmol·g⁻¹, respectively. The smaller amounts of the O₂ evolution are probably due to the presence of minor reaction of an ion-exchange adsorption. Equation 1 indicates that the Li⁺ insertion consumes an equivalent amount of OH⁻ ions. This is the reason why the Li⁺ insertion reaction could apparently be represented as the mechanism of an H⁺/Li⁺ ion exchange in the pH titration study in which only pH dependence of the Li⁺ uptake by λ -MnO₂ was measured.⁴⁾ Equation 1 also shows that

the Li^+ insertion in $\lambda\text{-MnO}_2$ proceeds through a unique reaction which involves the reduction of Mn(IV) and the oxidation of OH^- to O_2 . This unique reaction can be well explained on the basis of the concept of the one-phase solid redox system proposed by Kozawa et al.⁷⁾ Manganese oxide has the characteristics that small ions (H^+ , Li^+) and electrons (or positive charge) can move freely within the oxide structure to form a one-phase solid redox system. Therefore, the insertion reaction can be divided into two parts: 1) the insertion of Li^+ into a tetrahedral vacant site of the ccp oxygen framework of $\lambda\text{-MnO}_2$, accompanying a reduction of Mn(IV), and 2) the migration of excess positive-charge to the surface of $\lambda\text{-MnO}_2$ powder followed by the oxidation of OH^- in the aqueous phase.

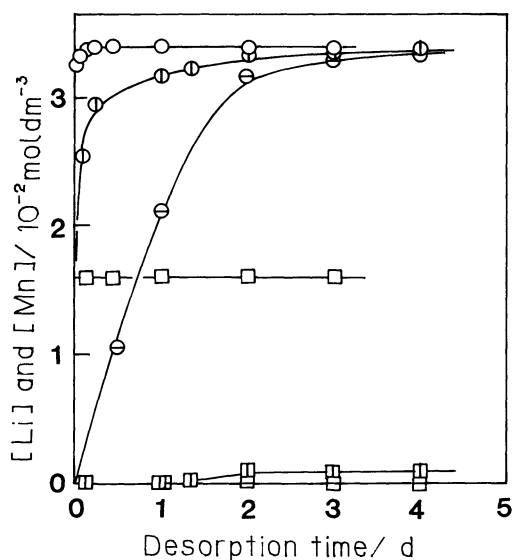


Fig. 3.
Time courses of Li^+ extraction at 25 °C. Circles and squares correspond to the concentrations of Li^+ and Mn, respectively.
Sample: $\lambda\text{-MnO}_2(\text{Li-II})$, 1 g, volume of soln.: 100 cm^3
O □: 0.2-M HCl, O ⊙: 0.1-M Br_2 ,
⊙ ⊙: 0.2-M $\text{K}_2\text{S}_2\text{O}_8$.

The rate of Li^+ extraction was rapid in a HCl solution: about 20 minutes was sufficient to reach equilibrium (Fig. 3). A dissolution of Mn was observed markedly in the HCl solution. The mole ratio of dissolved Mn to eluted Li^+ was 0.47, which is close to the expected ratio (0.5) in a Li^+ -extraction reaction from LiMn_2O_4 .¹⁾ In the case of oxidizing agents, the extraction of Li^+ could proceed with a slight dissolution of Mn. Samples after the extraction reaction maintained the same spinel structure as the original $\lambda\text{-MnO}_2$. A chemical analysis showed that most of the manganese was in a state of Mn(IV) after extraction (Table 1). These results suggest that the insertion/extraction of Li^+ proceeds reversibly in cooperation with a reduction/oxidation of manganese.

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